

# A continuous mashing system controlled by mean residence time

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# Abstract

Continuous processes offer more environmentally friendlier beer production compared to batch production. However, the continuous production of mashing has not become state-of-the-art in the brewing industry. The controllability and flexibility of this process still has hurdles for practical implementation, but which are necessary to react to changing raw materials. Once overcome, continuous mashing can be efficiently adapted to the raw materials. Both mean residence time and temperature were investigated as key parameters to influence the extract and fermentable sugar content of the wort. The continuous mashing process was implemented a continuous stirred tank reactor (CSTR) cascade consisting of mashing in (20°C), protein rest (50°C), β-amylase rest (62-64°C), saccharification rest (72°C) and mashing out (78°C). Two different temperature settings for the β-amylase rest were investigated with particular emphasis on fermentable sugars. Analysis of Variance (ANOVA) and post-hoc analysis showed that the mean residence time and temperature settings were suitable control parameters for fermentable sugars. In the experimental conditions, the most pronounced effect was with the β-amylase rest. These results broaden the understanding of heterogenous CSTR mashing systems including assembly and selection of process parameters.

#### Keywords:

Continuous mashing, continuous stirred tank reactor (CSTR), mean residence time, fermentable sugar.

# Introduction

Operations involved in beer production include malting, mashing, and fermentation. During mashing, carbohydrates and proteins in the malt are converted to simple sugars and amino acids by the enzyme in the malt. The hydrolysis of starch into fermentable sugars by enzymes such as α-amylase, β-amylase, limit dextrinase and α-glucosidase (Koljonen et al, 1995; Ziegler, 1999; MacGregor et al, 1999; Ma et al, 2000; Yin et al, 2002; Osman, 2002; Brandam et al, 2003; Bamforth, 2009; Gupta et al, 2010; Steiner et al, 2011; Quek et al, 2019; Wefing et al, 2020) is fundamental for subsequent alcohol production during fermentation by yeast. Accordingly, mashing can be described as a multi enzyme reaction system which also includes physical and chemical reactions. Furthermore, mashing has an impact on beer flavour and therefore on the consumers acceptance (Bamforth, 2009).

Globally, beer production is a batch process. Development of a continuous mashing process could contribute to more economic beer production (Strobl, 2020) provided that the process can be sufficiently controlled. The main advantages of continuous processes are (i) smaller reactors, pumps, heat exchanger, and valves; (ii) heat recovery; (iii) consistent energy consumption without peaks; (iv) reduced need for cleaning.

Continuous mashing processes have been explored since the 1920s (Silhavy and Saginaw, 1938; Cook and Davis, 1960; Watts et al, 1964; Hudson and Button, 1968; Huppmann, 1969; Kehse and Jess, 1974; Moll et al, 1976; Mulder, 2012; Mulder and Snip, 2018). However, the complexity of the mashing process has prevented stable industrial implementation. Reliable continuous systems have been established for processes before and after mashing, including milling, mash filtration, wort boiling, hot trub separation and the chilling/ aeration of wort (Willaert and Baron, 2001; Hertel and Sommer, 2016; Kempfert, 2016; Wefing et al, 2020). A suitably controlled continuous mashing process would be a significant development in an efficient continuous wort production that can adjust to the changing properties of raw materials.

The continuous mashing systems reported in literature include horizontal, vertical, plug-flow and continuous stirred tank reactors (CSTR) (Silhavy and Saginaw, 1938; Cook and Davis, 1960; Watts et al, 1964; Hudson and Button, 1968; Huppmann, 1969; Kehse and Jess, 1974; Moll et al, 1976; Mulder, 2012; Mulder and Snip, 2018). The implementation of a CSTR cascade would support a flexible continuous mashing, as the fill level of the individual continuous stirred tank reactors can be used to control sugar production in the process by altering the reaction time.

Continuous stirred tank reactors are typically controlled on the basis of mathematical modelling (Malar and Thyagarajan, 2009; Singh and Sharma, 2013; Bancila et al, 2021; Colbu et al, 2021). Numerous models describing the fermentable sugar formation by starch hydrolysis in the mashing process can be found (Muller, 1991; Koljonen et al, 1992, 1995; Brandam et al, 2003; Wefing et al, 2020). A semi-empirical, model proven to predict fermentable sugar concentration  $(c_{\text{rc}})$  in a continuously conducted β-amylase rest has been reported (Wefing et al, 2020):

$$
c_{rs}(t) = c_{rs,i} + C_{st,0} \cdot (1 - e^{-at})
$$
 (Eqn.1)

with α as:  $\alpha = (k_a \cdot \alpha_a + k_a \cdot \alpha_a + k_{LD} \cdot \alpha_{LD})$ (Eqn.2)

Here,  $c_{\text{rs}}$ , describes the concentration of fermentable sugar at the beginning of the mashing process, and  $C_{\text{sto}}$  the concentration of starch that can potentially be converted into fermentable sugars. The kinetic factors of the enzymes α-amylase, β-amylase, and limit dextrinase are represented by  $k_{a}$ ,  $k_{a}$ ,  $k_{L}$ , whereas the enzymatic activities of the enzymes are represented by  $\alpha_{a}$ ,  $\alpha_{b}$ ,  $\alpha_{\text{LD}}$ .

The concentration of fermentable sugars in the continuous β-amylase rest is then calculated by combining the residence time distribution (RTD), represented as exit age distribution E (Martin, 2000; Toftgaard Pedersen et al, 2017)

$$
c_{rs} = \int_0^\infty E(t) \cdot c_{rs}(t) \cdot dt \qquad (\text{Eqn.3})
$$

with: 
$$
E(t) = \frac{c_{tracer^{(t)}}}{\int_{t=0}^{t=\infty} c_{tracer^{(t)}dt}}
$$
 (Eqn.4)

The direct application of the model to control a mashing process is prevented by the hurdle that the RTD can only be determined by tracer experiments (Roussinova and Kresta, 2008). However, previous work provides the technological and scientific foundation for the application of the mean residence time to control the continuous mashing system described here. The mean residence time  $(t<sub>m</sub>)$  of the CSTRs can be altered by variation of (i) flow rate (V) and (ii) reactor volume  $V_r$  (De Ruyck, 1997; Roussinova and Kresta, 2008):

$$
t_m = \frac{V_r}{\dot{V}}
$$
 (Eqn.5)

In contrast to the RTD, the mean residence time  $(t_n)$ does not consider the design specific characteristics of a CSTR system. These characteristics include the reactor design, the inlet and outlet position, and mixing effects (Roussinova and Kresta, 2008). Accordingly, the mean residence time describes the average behaviour of a volume elements inside a CSTR with a lower quality than the residence time distribution. The mean residence time describes the average time a volume element lasts in a CSTR. Nevertheless, the mean residence time calculation is minor compared with the experimental effort for a RTD determination.

Therefore, if fermentable sugar concentrations can be controlled during mash production, the control of the continuous mashing process by the mean residence time may be reasonable.

Here, a novel continuous mashing system with a heterogeneous CSTR cascade enabling control of extract, maltose, and glucose levels was investigated. Various mean residence time settings, and other factors that influence the fluidic behaviour inside a CSTR were examined. Additionally, enzymatic conversion rates were considered as being affected by temperature changes.

In a continuous approach the three conversion steps in a conventional batch mashing process were considered. Firstly, (i) a protein rest optimised for β-glucan degradation by β-glucanase which is important with poorly modified malts (Wefing et al, 2020). Although normally performed at 48-52°C (Steiner et al, 2011), 38°C can be used (Jones and Marinac, 2002; Jones, 2005) with a final conversion step at 72°C (Jones and Marinac, 2002). The second phase (ii) - the  $β$ -amylase rest - performed at 62-65°C (Hui, 2007), with the third phase (iii) a saccharification rest, performed at 70-75°C (Hui, 2007). Additionally, a terminal production step, a continuous mashing out step was included (78°C).

The different temperature zones for the four mashing steps are considered as independent but inter-connected within the continuous stirred tank reactors (Figure 1).

#### Figure 1.

Schematic of the continuous mashing process and the RTD curves (for ideal CSTRs) that the different temperature zones can be interpreted as individual and completed reaction steps. Applying two CSTRs for the β-amylase rest changes the RTD curve for that process step.



Further, the number of reactors used for each temperature zone influences the RTD of the individual steps. In this study (Figure 1), a single CSTR and a CSTR cascade consisting of two reactors is alternatively used for the β-amylase rest stage. The different setups result in different RTD curve shapes for the production step, represented as the exit age distribution function *E(t)*. This affects the movement time of the volume elements through the system and plays a role in the understanding and evaluation of the controllability of the whole system.

This work uses the mean residence time as control parameter for the fermentable sugar content (maltose, glucose, and extract). Although an approximation, the mean residence time  $(t_n)$  may predict the 'real' mean residence time with varying accuracy for several CSTRs. The effect of different mean residence time settings was investigated by observing the fermentable sugar formation during the β-amylase rest, and at the end of the whole reactor cascade. Further, different temperature settings in the β-amylase rest stage were investigated to observe different starch conversation rates.

# Materials and methods

#### Mash preparation

For mash preparation, demineralised water (brewing liquor) and finely ground malt (Pilsner malt, Weyermann, Germany) was blended with finely ground unmalted barley (Ireks, Germany) at a ratio of 1:1. Unmalted barley has a lower enzymatic activity compared to malt. Therefore, a mixture of unmalted barley and malt has a reduced capacity for starch degradation compared to 100% malt. Consequently, longer mashing times are needed to compensate for the reduced starch degradation rate. This enables a continuous mashing system to use longer residence times.

Malt and barley were ground with a dynamic (rotor) impact mill (Mühlomat 100, Mück Sondermaschinenbau GmbH, Germany). A sieve analysis was conducted after blending malt and barley. The corresponding particle size distribution is reported in Figure 2. The grist liquor ratio of the

mash was 1:4 and the malt analysis is detailed in Table 1. The fine malt barley blend used in this work is equivalent to the malt reported in Wefing et al (2020).

#### Continuous mashing system

In this work, batch mashing consisted of a protein rest (48-52°C) (Steiner et al, 2011), β-amylase rest (62-65°C) (Hui, 2007) and saccharification rest (70- 75°C). This was transferred to a heterogeneous CSTR cascade laboratory-scale, self-constructed mashing system. Mashing-in (20°C) was also included. A schematic of the mashing system is shown in Figure 3A.

The continuous mashing system ('Smart Mashing Plant') consists of seven stainless steel reactors (Figure 3B). As an experimental platform, the number of CSTRs used for mashing can be changed. The mashing in CSTR volume was 2 L, while all the other CSTRs have a maximum volume of 1 L. The mash is pumped by peristaltic pumps. The internal diameter of the tubing is 4 mm. The flow rates were between 20 and 100 mL/min. The temperature settings of the CSTRs (the mashing in CSTR is not heated) is achieved by electrical heating. The continuous mashing system can deliver a beer mash production rate of 144 L/day.

# Figure 2.

Particle size distribution of fine malt and barley mixture (1:1) (Wefing et al, 2020).



## Figure 3A.

Continuous mashing system. The number of CSTRs for the β-amylase rest can be varied between one and two.





#### Figure 3B.

Continuous mashing enables variations in the CSTR cascade set up for continuous mashing trials.

## Continuous mashing trials

For the β-amylase rest stage in the continuous mashing process, several parameters were investigated - temperature (62 and 64°C), volume (300, 400, 600, and 800 mL) and number of reactors (one or two). Additionally, two different flow rates (60 and 100 mL/min) were chosen for the mashing trials. In all trials, the volume, the number of reactors and temperature were constant for the protein rest (500 mL, 50°C), saccharification rest (500 mL, 72°C) and mashing out (500 mL, 78°C).

The mash was mixed inside each continuous stirred tank reactor by oscillating agitators at a rate of 2.5Hz and a turning angle of 720°. When both CSTRs were used for the β-amylase rest, the volume of the CSTRs was:

$$
V_r = V_{\text{CSTR1}} + V_{\text{CSTR2}} \tag{5}
$$

To calculate the total mean residence time  $(t_{\text{m,total}})$ of the continuous mashing system, the combined volume of all used CSTRs was divided by the flow rate:

$$
t_{m, total} = \frac{\sum_{i}^{i} V_{CSTR,i}}{\dot{V}}
$$
 (6)

## Analytical methods

Samples were taken after the β-amylase rest and after mashing out. The samples were cooled immediately in a bath of ice water. Extract was determined using a refractometer (J157 Automatic Refractometer, Rudolph Research Analytical, USA). Maltose and glucose levels were determined by high performance liquid chromatography (HPLC). Sample preparation for the HPLC included (i) clarification with a Carrez kit, (ii) centrifugation at 2000g for 5 min, (iii) isolation of the supernatant and (iv) filtration of the supernatant through a 0.2 µm filter. A NH2-RP column (EC 250/4.6 Nucloeodur 100-3, Macherey-Nagel, Germany) was used at 30°C. Peaks were analysed using a RI detector (Shimadzu, Japan).

# Statistical analysis

Glucose and maltose levels are an average of three independent measurements. Extract is the average of six independent measurements. Error bars of the glucose and maltose values represent the span of values and with extract the standard deviation. The Shapiro-Wilk test was applied to check for a normal distribution of the data (Bee Wah and Mohd Razali, 2011). The effect of the mean residence time on extract, maltose and glucose concentration within

(i) β-amylase rest with one CSTR, (ii) β-amylase rest with two CSTRs, (iii) mashing out with one β-amylase rest CSTR and (iv) mashing out with two β-amylase rest CSTRs were analysed with a one-way analysis of variance (ANOVA) (Stohle and Wold, 1989; Osmekhina et al, 2010; Taskila et al, 2011; Bellut et al, 2018; Katsch et al, 2020, 2021). If p-values were above 0.05, Tukey's honestly significant difference (HSD) was used as post-hoc method (Marcinkowska-Lesiak et al, 2016; Bellut et al, 2018; Martinez-Amezaga et al, 2018; Katsch et al, 2021).

The effect of different temperatures on extract, maltose and glucose concentration was analysed by Student's t-test for two independent samples (Bee Wah and Mohd Razali, 2011; de Winter, 2013). All calculations were executed with python (version:3.8.5). The scipy stats (version: 1.8.0) libraries *scipy.stats.ttest\_ind* (Student's t-test), *scipy. stats.f\_oneway* (ANOVA), and *scipy.stats.shapiro* (Shapiro-Wilk test) were used for the calculations.

# Results

This work investigates whether the mean residence time can be used as a control parameter for extract, maltose, and glucose concentration in the continuous production of a beer mash. To show that this parameter is sufficiently sensitive to influence the concentration of fermentable sugars, volume and the flow rate were varied.

The results of mashing with a single β-amylase rest CSTR are presented in Figure 4 with the fermentable sugar levels against the CSTR volume (Figures 4A and B). The mean residence time  $(t_n)$  combines CSTR volume and flow rate allowing to represent results of the individual mashing trials (Figure 4C). As shown, the concentration of maltose, glucose, and extract increase as the mean residence time increases until reaching a plateau. This observation suggests that the mean residence time is sufficiently sensitive to be used as a control parameter in the mashing process.



#### Continuous **β**-amylase rest

#### Impact of mean residence time on sugar concentration

The mean residence time can be used to change the fermentable sugar concentration in the continuous mashing process. Two different temperature settings were used to assess variations in the temperature dependent conversion rate of the diastatic power enzymes (Table 2). A one-way ANOVA was applied, to compare the mashing trials with different mean residence times and the concentration of maltose, glucose and extract. If significant differences ( $p <$ 0.05) were found, Tukey's HSD test was applied. The results of the post-hoc-analysis are highlighted with letters beneath the data (Table 3).

The results with a single CSTR for the β-amylase rest at 62 and 64°C are shown in Figure 5. Trials with a mashing temperature of 62°C yielded the lowest maltose and extract concentration at the shortest mean residence times, with the highest values at the longest mean residence times. Similar conclusions were found when the β-amylase rest was conducted at 64°C (Figure 5). Only slight variations in glucose concentration were found with a single CSTR for the β-amylase rest.

In the 62°C mashing experiments, the different residence times resulted in a significant increase of the maltose concentration.

Tukey's HSD was used for a pairwise analysis and to categorise the different sugar levels ('A' to 'E') in Figure 5. With the 62°C trials only two significantly different levels of maltose were found (Figure 5A) and four different maltose levels were observed at 64°C (Figure 5B). This finding is consistent with the extract determination in both trials. Variation of  $t_m$  showed no effect on glucose levels for both temperatures. Therefore, extract together with maltose concentration can be controlled using the mean residence time with a single β-amylase rest CSTR. However, at 64°C the control was improved compared to 62°C.

The residence time distribution of a single CSTR was different to the RTD of two CSTRs in a cascade. Accordingly, it was investigated if the mean residence time is suitable as control parameter if a double CSTR setup is used for the continuous β-amylase rest (Figure 6). One way ANOVA revealed no significant differences in maltose and glucose concentration for the trials at 62 and 64°C. However, the extract was found to show significant differences at both temperatures. At 62°C, the highest extract value was reached with  $t_m = 13.3$  minutes. When continuous mashing was conducted at 64°C, no significant increase of sugar levels was found for  $t_{m}$ values higher than 8 minutes. When two CSTRs in cascade are used for the β-amylase rest, the extract can be controlled by the mean residence time. Posthoc-analysis within  $p < 0.05$  showed no significant difference in levels of glucose and maltose.



#### Table 2.

**Continuous** β-amylase rest mashing trials.

# Table 3.

Significance analysis of changes affected by the mean residence time in continuous β-amylase rest trials.



1 CSTR. B-Amylase rest

#### 2 CSTRs, β-Amylase rest



#### Figure 5.

Extract, maltose, and glucose concentrations in the continuous β-amylase rest with a single CSTR. **A**: β-amylase rest temperature = 62°C;

**B**: β-amylase rest temperature = 64°C. Letters 'A' to 'E' represent the significant differences between the extract, maltose and glucose levels based on an ANOVA analysis with Tukey's HSD as post-hoc test with significance level p < 0.05; Maltose and glucose:  $n = 3$ , error bars: span of values: extract:  $n = 6$ , error bars: standard deviation.



#### Figure 6.

Extract, maltose, and glucose concentrations in the continuous β-amylase rest with a cascade of two CSTRs. **A**: β-amylase rest temperature = 62°C; **B**: β-amylase rest temperature = 64°C. Letters 'A' to 'C' represent significant differences between the determined extract, maltose and glucose levels based on an ANOVA analysis with Tukey's HSD as post-hoc test with significance level  $p < 0.05$ ; Maltose and glucose:  $n = 3$ , error bars: span of values; extract:  $n = 6$ , error bars: standard deviation.



## Impact of temperature on sugar levels in β-amylase rest

The mashing trials were influenced by the selected β-amylase rest temperatures. Therefore, experiments were designed to explore the impact of different temperature settings on the continuous mashing process. Mashing trials with equal mean residence times but conducted at different temperatures were compared. The resulting extract, maltose, and glucose concentrations were analysed by the aid of Student's t-test. The results are shown in Table 4 and Figure 7.

With a single CSTR for the continuous β-amylase rest, the different temperature settings significantly (p < 0.05) influenced the extract levels (Figure 7A). This was also found for maltose within a significance level of  $p < 0.10$ . Except for  $t_m = 3$  minutes, changes in maltose concentration were found with a significance level of  $p < 0.05$ . Similarly, glucose concentration was significantly changed ( $p < 0.05$ ) at the different temperature settings.

Because of the lower proportion of glucose in the mash compared to other fermentable sugars (Koljonen et al, 1995; Fox, 2016), the differences in glucose were small compared to the differences in maltose concentration, Furthermore, the use of two CSTRs in a cascade for the β-amylase rest showed that the different temperature settings significantly affect extract levels (Figure 7B). Accordingly, the use of temperature as a control parameter is appropriate to change extract levels regardless of the number of CSTRs used for the β-amylase rest. If a single CSTR is used, both maltose and glucose concentration can be controlled by temperature.

## Figure 7.

Comparison of extract, maltose, and glucose concentrations in continuous β-amylase rests conducted at 62 and 64°C. **A**: single CSTR;

**B**: two CSTRs in a cascade. The p-value describing the temperature effect (62/64°C) was determined by Student's t-test; Malt to liquor ratio: 1:4.



#### Continuous mashing process

#### Impact of the mean residence time on sugar concentration

In the continuous mashing process, most of the fermentable sugars are formed by the diastatic enzymes during β-amylase rest. To clarify if the saccharification rest and mashing out are influenced by the β-amylase rest, the mash was sampled at the end of the mashing process.

The mean residence time can be influenced by either the reactor volume or the flow rate. A flow rate change influences the mean residence time in all the interconnected CSTRs. Accordingly, a flow rate of 60 mL/min results in a combined mean residence time of 25 minutes for the protein rest (50°C), saccharification rest (72°C), and mashing out (78°C). If the flow rate is 100 mL/min, the combined mean residence time for the protein rest, saccharification rest and mashing out is 15 minutes. The total mean residence time  $(t_{\text{m,total}})$  results from combining the mean residence time of the β-amylase rest, protein rest, saccharification rest, and mashing out.

The results obtained previously showed that a single β-amylase rest CSTR effects different fermentable sugar levels along with a different degree of controllability compared to the double stage β-amylase rest CSTR. Therefore, both variants were examined individually regarding their effect on the overall mashing process.

Significant differences for maltose, glucose, and extract concentration were found with a single CSTR used for the β-amylase rest (Figure 8, Tables 5 & 6). Tukey's HSD analysis showed with a single CSTR for the β-amylase rest at 62°C, the glucose concentration was lowest at the longest residence time. Glucose values at shorter residence times showed no significant difference.



#### Figure 8.

Extract, maltose, and glucose concentrations at the end of the continuous mashing process with a single CSTR for the β-amylase rest.

**A**: β-amylase rest temperature = 62°C, flow rate: 100 mL/min and 60 mL/min; **B**: β-amylase rest temperature = 64°C, flow rate: 100 mL/min and 60 mL/min; Letters 'A' to 'E' show significant differences between the determined extract, maltose and glucose levels (ANOVA analysis with Tukey's HSD as post-hoc test with significance level  $p < 0.05$ ); n = 3, error bars: span of values; extract: n = 6, error bars: standard deviation.

#### Table 3.

#### Results of continuous mashing trials.



#### Table 6.

#### Significance analysis of changes affected by the mean residence time in continuous mashing trials.



#### 1 B-Amylase rest CSTR, Mashing out

#### 2 β-Amylase rest CSTRs, Mashing out



However, ANOVA confirmed that  $t_{m,total}$  had no significant influence on glucose, if the β-amylase rest was performed at 64°C. Five different extract levels were found when the β-amylase rest was at 62°C and three when the mashing temperature was set to 64°C. Different mean residence times also led to significantly different maltose levels for both β-amylase rest temperatures. No significant differences in glucose and maltose concentration were found at the end of the mashing process (Figure 9). Extract determination showed that significant changes in extract levels can be introduced by mean residence time regardless of the temperature of the β-amylase rest.

Mean residence times in the range of 3 to 5 minutes applied to the β-amylase rest stage resulted in the lowest extract levels after mashing out. This observation was independent whether a single CSTR or a double reactor cascade was used. Fermentable sugar concentrations were increased after saccharification and mashing out but did not reach the levels found with longer mean residence times in the β-amylase rest. Different mean residence times with the β-amylase rest showed an effect on extract and maltose concentration and can be assumed as a control parameter. However, the effect was increased when a single CSTR for the β-amylase rest was used.



#### Figure 9.

Extract, maltose, and glucose concentrations at the end of the continuous mashing process with two CSTRs in a cascade for the β-amylase rest.

**A**: β-amylase rest temperature = 62°C, flow rate: 100 mL/min and 60 mL/min; **B**: β-amylase rest temperature = 64°C, flow rate: 100 mL/min and 60 mL/min; Letters 'A' to 'D' show significant differences between the determined extract, maltose and glucose levels (ANOVA analysis with Tukey's HSD as post-hoc test with significance level  $p < 0.05$ ); Maltose and glucose:  $n = 3$ , error bars: span of values; extract:  $n = 6$ , error bars: standard deviation.

# Impact of temperature on sugar levels during β-amylase rest

As different temperature settings in the β-amylase rest stage show significant impact on fermentable sugar concentrations, its effect on the overall process was investigated. Therefore, mash samples with the same mean residence time were taken at the end of the process.

As shown in Figure 10 and Table 7, a significant difference ( $p < 0.10$ ) in extract concentration was found for all the samples. Additionally, significant differences in extract levels ( $p < 0.05$ ) were found for all the mean residence times, with the exception of  $t_{m,total}$  = 38.3 minutes. Furthermore, due to temperature changes, maltose levels can be significantly influenced (p < 0.05) where a single CSTR is used for the β-amylase rest.

Glucose level remained unaffected by different temperatures, with two exceptions: a single CSTR for β-amylase rest was used with residence times  $t_{m, total}$  = 23 and 38.3 minutes. However, when two CSTRs were used in a cascade for the β-amylase rest, different temperatures had no significant effect on maltose and glucose levels.

In conclusion the examined temperatures can be used to control extract levels, independent from the number of β-amylase rest CSTRs and mean residence time. In contrast, glucose and maltose concentrations are only significantly affected, when a single CSTR is used for the β-amylase rest.



## Figure 10.

Comparison of extract, maltose and glucose levels concentrations at the end of the continuous mashing process with the continuous β-amylase rest conducted at 62 and 64°C.

**A**: single β-amylase rests CSTR; **B**: two β-amylase rests CSTRs in a cascade. t<sub>m</sub> is the mean residence time; the p-value describing the temperature effect (62/64°C) was determined by Student's t-test.

#### Table 7.

Student's t-test analysis to determine significant differences affected by the mashing temperature in the continuous β-amylase rest.



1 β-Amylase rest CSTR, Mashing out, 62°C/64°C

# Discussion

The key to successful continuous mashing is the capability to adapt to the raw materials used for mashing. Barley malt to is prone to environmental and genotypic variations that alter its characteristics (Dai et al, 2007; Cai et al, 2013; Henson et al., 2014). All existing continuous mashing systems are broadly inflexible and cannot react on changing raw material properties in the process (Silhavy and Saginaw, 1938; Cook and Davis, 1960; Watts et al, 1964; Hudson and Button, 1968; Huppmann, 1969; Kehse and Jess, 1974; Moll et al, 1976; Mulder, 2012; Mulder and Snip, 2018)

Here, it was demonstrated, that the CSTR mashing system can control extract and maltose levels via mean residence time. The mashing system consists of a series of steps; protein rest, β-amylase rest, saccharification rest and mashing out. The influence of the individual process steps are discussed in terms of their impact on the fermentable sugar concentration.

The mean residence time was altered by variation in the fill level of the CSTR in the β-amylase rest and by changing the flow rate. As changes in flow rate impact the mean residence time of the process steps, it is necessary to understand its impact on each step.

Additionally, it was demonstrated that the fermentable sugar concentration can be altered by changing the temperature of the β-amylase rest stage temperature. This allows for a second control parameter in the continuous mashing system besides mean residence time.

## Protein rest

In practice, unless poorly modified malt is used, the protein rest is excluded. However, the protein rest was included in the continuous process. A change in the flow rate and the mean residence time of the protein rest had no influence on the formation of maltose, glucose, or extract. This was to be expected as the temperature of the continuous protein rest was 50°C and below that required for gelatinisation of starch. Gelatinisation of mash is an important precondition for the starch degradation (Brandam et al, 2003). Fox et al (2019) reported typical onset gelatinisation temperatures for malt in a range of 54.2 to 60.5°C and for barley in a range between 56.6 to 62.0°C. It is noteworthy that Evans and Fox (2017) found that β-amylase activity during long resting times can be increased by mash temperatures between 45 to 55°C compared to the mashing process without a protein rest. However, this was not found here perhaps because of the short residence time used for the continuous mashing compared to a batch process. Further, changes in the mean residence time during the protein rest is anticipated to influence levels of free amino nitrogen, and the fermentability of the wort. An impact on haze and foam stability of the subsequent beer is possible by reducing the overall length of high molecular weight proteins in the mash (Montanari et al, 2005; Steiner et al, 2011).

## β-amylase rest

One of the main aims of this study was whether the mean residence time was sufficiently sensitive as control parameter for a continuous mashing process. The major contribution to fermentable sugars is provided by the β-amylase rest (Henson et al., 2014) and this stage was observed in detail. The enzymes contributing to sugar formation by starch hydrolysis at 62°C to 64°C include α-amylase, β-amylase and limit dextrinase (Evans et al, 2005; Evans and Fox, 2017). The impact of temperature and time on starch degradation has previously been investigated (Jones and Marinac, 2002; Montanari et al, 2005; Wijngaard and Arendt, 2006; Durand et al, 2009). A direct comparison of batch and continuous processes is difficult but, as an approximation, the mean residence time and batch rest time can be compared.

While in a batch process it is assumed that temperature and time are the same, there is a degree of heterogeneity due to the ineffective mixing of the grist. In a continuous process the mean residence time describes how long an element (eg volume) remains in a CSTR on average (Toson et al, 2019), but is an approximation of how long the 'average volume element' remains in a CSTR. Other volume elements remain longer or shorter in the reactor than indicated by the mean residence time.

The amount of mash leaving the CSTR before or after the estimated mean residence time is dependent on the reactor's flow setting, the geometry, and the number of reactors. The RTD, representing the statistical behaviour of all volume elements can be determined by tracer experiments (Tsai and Chen, 2013; Igbokwe et al, 2015). Such experiments are only suitable to predict the RTD depending on a specific set of settings such as flow rate and reactor volume. However, these experiments are costly and time consuming and are not practical for industrial processes.

Extract concentration within the trials conducted with a single CSTR followed a similar rise, due to increased mean residence times. This was expected as maltose is a major contributor to extract (Fox, 2016). Accordingly, the concentration of maltose and extract are influenced by the mean residence time and the effect is greater at higher temperatures.

Results of continuous mashing with a CSTR double cascade (only β-amylase rest) are at a first glance contradictory to the results obtained with a single CSTR. Indeed, significant changes in extract levels were found if the residence time was altered but no significant changes in maltose levels were observed  $(p < 0.05)$ . However, the mean maltose values showed a trend that is comparable to the extract concentrations, which is increasing in response to altered residence time settings for both tested temperatures. Significant differences were found for the maltose values only with a confidence level of p < 0.10 (opposed to the confidence level of p < 0.05 used for single CSTR). No significant changes with a  $p < 0.05$  were found. This may be due to unavoidable measurement errors. The reason for the relatively minor differences between maltose and extract levels when applying short residence

times might be due to the behaviour of individual volume elements inside the CSTR. As noted above, with two CSTRs in a cascade, the residence time most likely is longer than the calculated mean residence time  $t_m$ . That can also explain how higher maltose concentrations were found for the cascade compared with the single CSTR at similar residence times.

#### Overall mashing process

As mashing at 65°C and 72°C converts starch into fermentable sugars (Jones and Marinac, 2002) the extract, and maltose concentration obtained in the continuous β-amylase rest influence the amount of fermentable sugars formed by the saccharification rest. Indeed, any deficiencies in starch conversation due to shorter mean residence times during the β-amylase rest can be compensated for by the saccharification rest. This was confirmed by mashing at 62°C where the double CSTR cascade reached levels of extract and maltose in the range of mashing at 64°C.

The conversion of starch during the saccharification rest is distinct to the β-amylase rest. The activities of limit dextrinase and β-amylase are increasingly impaired at 72°C (Evans and Fox, 2017), with no β-amylase activity after 30 minutes at temperatures of  $\geq$  68°C (Henson et al., 2014). With mean residence times beyond 30 minutes during the continuous β-amylase rest, it is unlikely that β-amylase and limit dextrinase contribute to sugar levels in the saccharification rest at temperatures ≥ 72°C. Accordingly, the results with different mean residence times during the β-amylase rest are only relevant if low extract and maltose levels are targeted in the mashing process. Changes in the volume of the saccharification rest and mashing out were not applied in this study but may contribute to the control of fermentable sugar levels during continuous mashing and should be further investigated.

## Temperature effect in the continuous β-amylase rest

Different temperature settings for the continuous β-amylase rest showed that it can be used as control parameter in a continuous mashing process. Also, it can be assumed that longer reaction times are able to compensate for lower temperatures during the β-amylase rest. This was observed as the different temperatures showed the most pronounced differences when applying the shortest residence times (highest flow rates). On the other hand, with increasing mean residence times, this was not significant with maltose and glucose levels and limited with extract. The increased sugar concentration obtained in the 64°C β-amylase rest reflect higher enzyme activities. Notably, starch degradation depends on the interplay of several different enzymes (Bamforth, 2003; Evans et al, 2005) where higher sugar levels do not reflect the activity of a single enzyme. However, the elevated temperature may have increased the enzymatic activity of the diastatic power enzymes ( $\alpha$ -amylase, β-amylase, limit dextrinase).

The applied mean residence times for the β-amylase rest (3-13.3 minutes) were short compared to the batch process. Therefore, the heat inactivation of enzymes may not have been significant. Indeed, Evans and Fox (2017) found that β-amylase activity in malt mashes declines at 65°C by 50% within 60 minutes (Evans and Fox, 2017). Surprisingly, in the same study, limit dextrinase activity was demonstrated to increase for the first 20 minutes at 65°C (Evans and Fox, 2017). However, this observation was made with a grist:liquor ratio of 1:3, with Evans and Fox (2017) reporting that thicker mashes might be less temperature dependent on enzyme activity.

If at 65°C, half the activity of β-amylase is lost (Evans and Fox, 2017), then the short mean residence time in the mashing trials had little impact on enzymatic activity. Nonetheless, the plateau of extract and maltose values at 64°C with a single CSTR were higher compared than at 62°C. A decrease of enzymatic activity either by inhibition or inactivation may explain these results. This was confirmed by the double CSTR cascade for β-amylase rest showing the highest extract and maltose levels at their respective temperatures.

# Conclusions

This study demonstrates that a continuous β-amylase rest in a CSTR can be controlled by mean residence time. The range of mean residence times for the β-amylase rest was three to 13.33 minutes. The continuous β-amylase rest at 64°C allowed a finer adjustment of fermentable sugar levels than at 62°C. If with the β-amylase rest, the mean residence time was low, low fermentable sugar levels in the β -amylase rest were compensated for by the subsequent process steps. It was also demonstrated that temperature as control parameter can be applied in a continuous mashing process. At shorter residence times, the effect of temperature was greater compared to the effect of the extension of the residence times. Currently, the continuous mashing system used in this study is not fully controllable by the mean residence time. If the mean residence time is low, temperature is a suitable control parameter to affect the fermentable sugar concentration.

# Author contributions

**Patrick Wefing**: conceptualisation (lead); investigation (lead); methodology; writing (original draft); writing – review and editing (equal); formal analysis; software; visualisation.

**Marc Trilling**: conceptualisation; investigation.

**Arthur Gossen**: investigation.

**Peter Neubauer:** writing (review and editing) (equal).

**Jan Schneider:** writing (review and editing) (equal); supervision; conceptualisation.

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# Conflicts of interest

The authors declare no conflict of interest. The funders had no role in the design of the study, the collection, analyses, or interpretation of the data and in the writing of the manuscript.

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